

SITE - PREP

#### Lo Pro MODEL 427CM





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## FOOTING RECOMMENDATIONS

Adequate footings must be provided prior to set-up of plant. See plant assembly drawing, for column loadings, obtain a soil test and consult a professional Engineer for foundation design.

#### **IMPORTANT:**

BECAUSE OF THE RELATIVELY LARGE LOADS IMPOSED ON THE FOOTINGS, THE ALLOWABLE BEARING PRESSURE OF ALL UNDERLYING SOIL SHOULD BE DETERMINED AND OR CONFIRMED PRIOR ΑN APPROPRIATE **FOOTING** DESIGN. DUE CONSIDERATION FOR SETTLEMENT SHOULD BE INVESTIGATED INCLUDING THE POSSIBILITY OF A SOFT COMPRESSIBLE LAYER OF SOIL BENEATH THE TOP LAYER OF SOIL, AND ANY OTHER CHARACTERISTICS THAT MIGHT CAUSE EXCESSIVE SETTLING OR THE LACK OF SETTLEMENT. ADEQUATE UPLIFT RESTRAINT COULD CAUSE A DANGEROUS CATASTROPHE WITH COSTLY STRUCTURAL DAMAGE.

The customer is required to furnish steel leveling plates of no less than 3/4" x 10" x 10" material for each column required. If plant is to be permanently located CON-E-CO recommends installation of additional footings and piers to accommodate future expansion of bins.

NOTE: Portable footings may be used, if a reputable professional engineer is consulted for design of the portable footings.



## SPECIAL BRACING REQUIREMENTS

CON-E-CO structural supports, are designed for normal wind and adequate foundations. It may be necessary in some locations to provide additional bracing in order to comply with the design criteria of local codes for hurricane force winds or seismic loadings.

## **CHARGING RAMPS AND BUILDING**

Charging ramps and buildings should be free standing and not dependent on the plant for structural support. CON-E-CO assumes no responsibility for damage to a plant caused by a charging ramp or building.

## WATER REQUIREMENTS

The plant water may be obtained from city systems, well or surge tank. A minimum flow rate of approximately 100 to 150 GPM is advisable in order to maintain batching speed. CON-E-CO water meter will operate with much lower flow rates if required, approximately 30 GPM for 2" meter or 50 GPM for 3" meter. CON-E-CO recommends that a maximum pressure of 150 PSI not be exceeded. (The CON-E-CO water meter will handle water at temperatures ranging from 32 degrees F to 200 degrees F.) See Page 2 showing with without location. (Location Will waterline shown work or CON-E-CO furnished water pump.)

## **GENERAL NOTES**

CON-E-CO Structures are all designed to be mounted on level, rigid foundations. All foundations, permanent or temporary, must not allow more than 1/2" differential settlement or uplift between columns during or after repeated wind and/or live loads. Foundation loads are shown from specific plant configurations in site preparation drawings supplied by CON-E-CO. Added accessories such as cement silos, water tanks, conveyors, and dust control systems which are not shown on the plant's site preparation drawing cause higher stresses on the plant and larger foundation loads and/or uplifts. Consult CON-E-CO before adding anything to a plant not shown on its site preparation drawing.



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#### SPECIFICATIONS FOR MODEL PJC-32 CARTRIDGE DUST CONTROL

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#### MODEL CON-E-CO-PJC-32

NUMBER OF CARTRIDGES NOMINAL CARTRIDGE DIAMETER NOMINAL CARTRIDGE LENGTH TOTAL FILTRATION AREA MIN. DESIGN EFFICIENCY OF DUST COLLECTOR AIR TO CLOTH RATIO CAPACITY FOR CEMENT DISCHARGE AREA DISCHARGE VELOCITY @1500 C.F.M. DIRECTION OF AIR DISCHARGE DISCHARGE SHAPE NORMAL OPERATING DISCHARGE TEMP & PRESSURE AMBIENT **OUTLET MOISTURE CONTENT CLEANING MECHANISM** FREQUENCY OF CLEANING

16" 32.4 SQ. FT. 99.9% 5.0 TO 1.0 (CEMENT) 162 C.F.M. .20 SQ. FT. 13.5 FT. / SEC. DOWN WARD 13/16 X 35.5" SLOTS **IDEALLY ZERO PULSE JET** 

**VARIABLE** 

#### CARTRIDGE SPECIFICATIONS

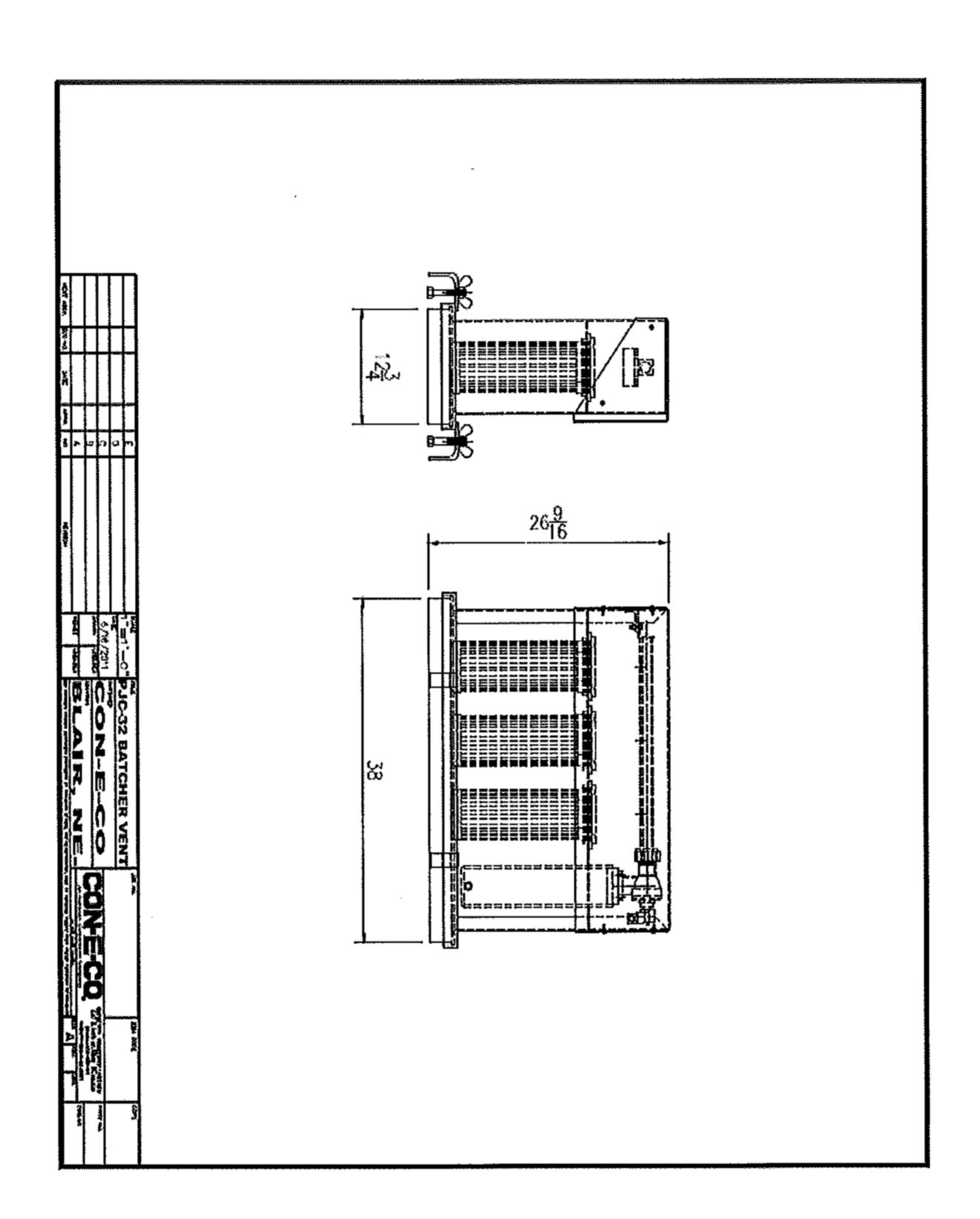
CARTRIDGE DIAMETER CARTRIDGE LENGTH CONSTRUCTION FIBER WEIGHT PERMEABILITY (.5" WATER) 6" O.D. 16" PLEATED SPUNBOND POLYESTER 8 OZ / SQ. YD. 24 CFM/SQ FT



















**PJC Series Batcher Filter Vent** 

**MAINTENANCE & OPERATION** 

#### **OPERATION**

The CON-E-CO Pulse Jet Cartridge Series Silo Filter Vents are designed for continuous operation and cleaning when batcher is being discharged.

#### **CARTRIDGE CHAMBER**

Contaminated air enters from the bottom of the cartridge chamber and flows from the outside toward the inside of the cartridges, leaving dust particles on the outside of the cartridges. Clean air exits through the top.

#### **CARTRIDGE CLEANING**

A pulse jet valve is mounted on a manifold on the batcher vent and controls air to the blowpipe located above the row of pulse jet cartridges. Holes in the blowpipe centered over each cartridge opening direct air downward through a venturi into the cartridges.

Cleaning of the cartridge is accomplished by a jet of air directed downward into the cartridge. The jet of air is short duration, high velocity and directs enough air volume to reverse the flow of air for a very short time to dislodge the dust from the outside of the cartridge.

#### **AIR PRESSURE**

Air pressure at the manifold (located on the filter vent) should be maintained at 90 to 100 psi. Less than 90 psi will reduce cleaning efficiency: Greater than 100 psi will cause excessive cartridge wear.

#### CONTROL

The pulse jet valve is controlled by an adjustable timer (see electrical print) located in the plant service panel. The timer is installed to receive a signal from the limit switch located on the batcher discharge gate. When the discharge gate opens and the closed signal goes away the timer will send a signal to the pulse jet valve to pulse.

#### **INITIAL SETTING**

The timer should be set to 0.125 seconds.

ON TIME less than 100 milliseconds will result in ineffective bag cleaning ON TIME greater than 200 milliseconds will result in excessive air usage

#### BATCHER VENT CARTRIDGE MAINTENANCE

The vent cartridges should be removed and inspected for tears or excessive buildup of material.

A visual inspection of the discharge air from the batcher vent at the time of weigh up should be made on a daily basis. If it appears that dust is escaping the filter cartridges they should be removed for a visual inspection.

Regular inspection of the filter vent should be at a maximum of six month intervals. General inspection of wiring, condition of door gaskets and caulked connections should be made. Also the filter cartridges should be removed for a visual inspection at this time.









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#### **SPARE PARTS**

Parts should be ordered from manufacturer to insure compatibility. If parts are needed, obtain serial number from the name plate and call the factory. A complete detailed record of the vent is on file at CON-E-CO.

#### SAFETY INFORMATION

This CON-E-CO dust collector, like other industrial equipment, must be operated and maintained in accordance with our instructions and sound engineering practices. The user of this equipment must always be aware of the physical and chemical properties of the dust particles being collected. Materials or processes presenting such hazards must be identified by the user.











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#### SPECIFICATIONS FOR MODEL PJ-980D DUST COLLECTION SYSTEM

MODEL CON-E-CO PJ-980D

66 NUMBER OF BAGS 6" NOMINAL BAG DIAMETER 120" NOMINAL BAG LENGTH

980 SQ. FT. TOTAL FILTRATION AREA MIN. DESIGN EFFICIENCY OF DUST COLLECTOR 99.9%

6.0 TO 1.0 AIR TO CLOTH RATIO 15 HP BLOWER HP

9" (INCHES OF WATER) STATIC PRESSURE DROP

5880 C.F.M. **BLOWER AIR FLOW** 60.7 FT. / SEC. DISCHARGE VELOCITY 1.60 SQ. FT. DISCHARGE AREA HORIZONTAL

DIRECTION OF AIR DISCHARGE

11 1/2" X 20" RECTANGLE DISCHARGE SHAPE

NORMAL OPERATING DISCHARGE TEMP & PRESSURE AMBIENT **IDEALLY ZERO** OUTLET MOISTURE CONTENT **PULSE JET** CLEANING MECHANISM VARIABLE FREQUENCY OF CLEANING

**BAG SPECIFICATIONS** 

5.93" BAG DIAMETER 121° **BAG LENGTH** SEAMED CONSTRUCTION

POLYESTER FELT **FIBER** SINGED FINISH 16 OZ / SQ. YD. WEIGHT 20-30 CFM PERMEABILITY (.5" WATER)

2.5 DENIER AVERAGE FIBER SIZE

BATCH PLANT DUST EMISSIONS CALCULATIONS INTO BAGS

CEMENT SILO

INTO BAGS .177 LB/YD<sup>3</sup> \* \_\_\_YD<sup>3</sup>/HR LB / HR .020 GR HR/LB FT<sup>3</sup>\* LB/HR GR / FT<sup>3</sup>

**INTO BAGS** FLYASH SILO .115 LB/YD<sup>3</sup> \* \_\_\_YD<sup>3</sup>/HR LB / HR

.020 GR HR/LB FT<sup>3</sup> \* LB/HR GR / FT<sup>3</sup>

CENTRAL MIX

 $.153 LB/YD^3 * ___YD^3/HR$ LB / HR .020 GR HR/LB FT<sup>3</sup>\* LB/HR GR / FT<sup>3</sup>

TRUCK MIX .281 LB/YD<sup>3</sup> \* \_\_\_YD<sup>3</sup>/HR LB / HR

.020 GR HR/LB FT3 \* \_\_\_LB/HR GR/FT<sup>3</sup>

**OUT OF BAGS** 

FOR ALL OUT OF BAGS VALUES, MULTIPLY THE INTO BAGS VALUES BY .001.



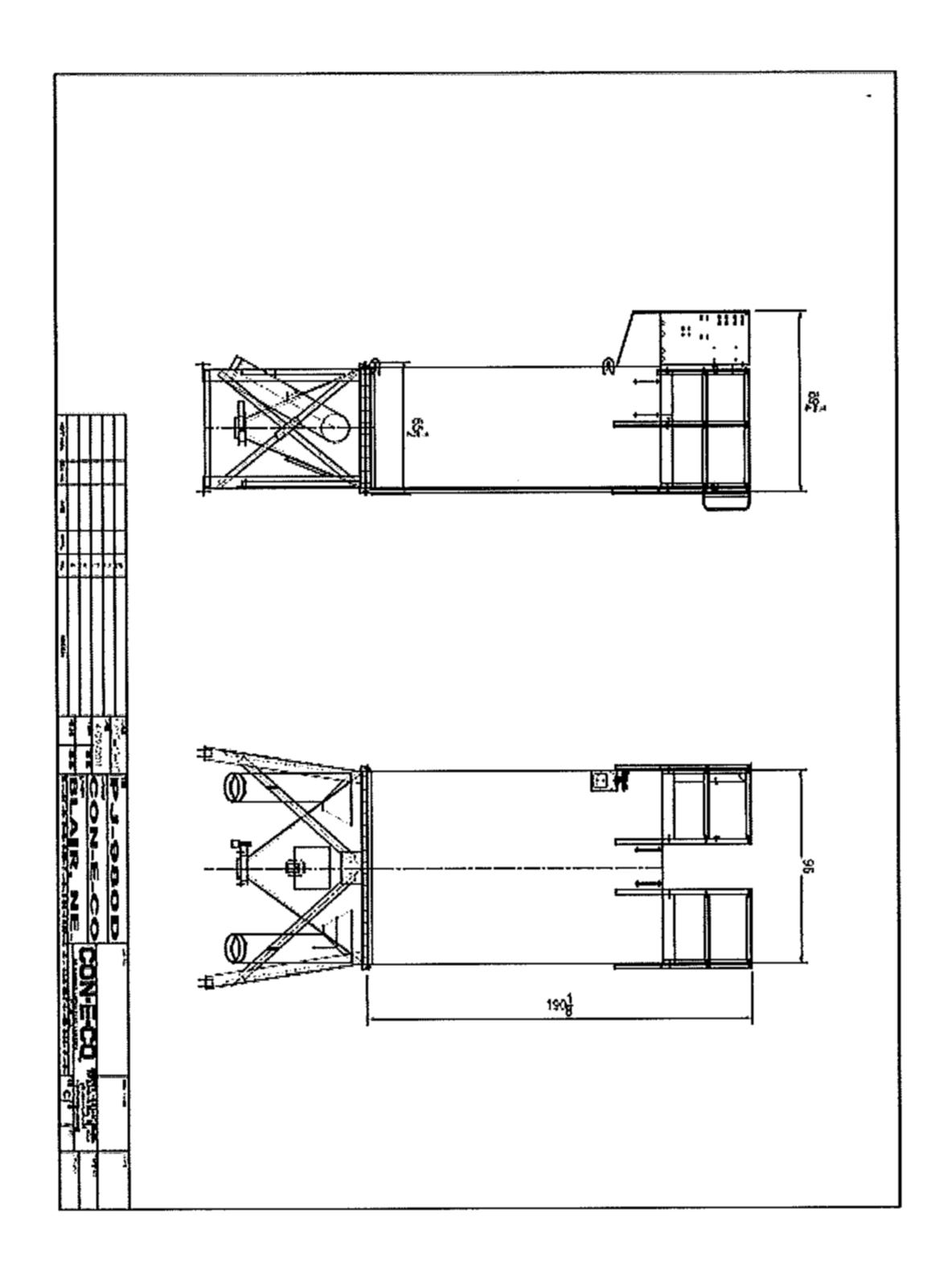






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#### PJ Series Central Dust Collector MAINTENANCE & OPERATION

#### **OPERATION**

The CON-E-CO Pulse Jet Series Dust Collectors are designed for continuous operation and cleaning. Contaminated air enters the dust collector, either through the collection hopper or the built in side plenum.

#### **INTAKE AIR**

Contaminated air enters the dust collector through the lower dust collection hopper. In this chamber, many of the heavy dust particles settle out of the air stream into the hopper bottom due to a reduction of air velocity.

If an intake duct connects to the top or side of the dust collector the dust laden air is connecting to the internal side plenum. From here the dusty air flows down into the hopper before turning and flowing up into the bag chamber.

#### **BAG CHAMBER**

Contaminated air enters from the bottom of the bag chamber and flows from the outside toward the inside of the bags, leaving dust particles on the outside of the bags. Clean air exits through the top where it is discharged by the blower.

#### **BAG CLEANING**

Cleaning of the bags is done one row at a time. Pulse jet valves are mounted on a manifold inside the bag house and control air to the blowpipes located above the rows of bags. Holes in the blowpipes centered over each bag opening direct air downward through a venturi into the bags.

Cleaning of the bags is accomplished by a jet of air directed downward through a venturi into the bags. The jet of air is short duration, high velocity and directs enough air volume to reverse the flow of air for a very short time to dislodge the dust from the outside of the bag.

#### AIR PRESSURE

Air pressure at the manifold (located inside the baghouse) should be maintained at 90 to 100 psi.

Less than 90 psi will reduce cleaning efficiency: Greater than 100 psi will cause excessive bag wear.







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#### CONTROL

The pulse jet valves are controlled by an adjustable solid state timer board. (See timer instruction for technical and programming instructions) This timer board controls several functions as described below:

ON TIME Pulse duration: Time that a pulse jet valve is open

ON TIME less than 50 milliseconds will result in ineffective bag cleaning

ON TIME greater than 300 milliseconds will result in excessive air usage

OFF TIME Time between pulses:

Reducing the "OFF TIME" will keep the bags cleaner and decrease bag life. Increasing the "OFF TIME" will allow more dust cake and increase bag life. The best way to obtain optimum performance is to measure the partial vacuum.

above the bags, maintaining negative pressure of 4" to 7" of water.

#### INITIAL SETTINGS

The dust collector timer control should initially be set as shown below. These settings should give the best balance of cleaning efficiency, air efficiency, and bag life for most common applications.

ON TIME

150 milliseconds

OFF TIME 30 seconds

#### **MAGNEHELIC GAUGE**

The control panel is equipped with a magnehelic gauge which measures the partial vacuum above the bags in the baghouse. High readings indicate high resistance to air flow through the bags (dust covered bags). Low readings indicate low resistance to air flow (clean bags).

It should be noted that the bags will require several weeks to establish a nominal operating pressure. This is because it takes time for the filter media to establish a small even coating on the bag skin to reach maximum operating effectiveness

### FIELD OPERATION

Recommended operation of a PJ Series Central Dust Collector is as follow:

Blower Operation: The blower of the dust collector should be on whenever the mixer is being loaded or when loading silos/bins with central dust collector. It is not recommended that the blower is switched off after every load, if continuous loading is expected. Frequently starting and stopping of blower with cause increased wear and premature failure.

Pulse (Cleaning) Operation: The cleaning cycle of the dust collector should be activated whenever plant power in turned on. It is recommend that the cleaning operation of the bags continues for 5-10 minutes after the blower has turned off, this will allow for more efficient clean of the bags.

Discharge of Waste Material (Reclaiming): The frequency in which the reclaim hopper needs to be emptied is determined on a case by cases basis. The larger the volume of concrete produced by the plant the more often it needs to be emptied. Upon initial use of the dust collector the hopper should be emptied daily to determine the amount of material being generated and it is recommended that you should reclaim no more than 200-300 lbs at a time. If you reclaiming more than this amount the frequency needs to be increased.

With a reclaim system that blows the material into a silo a weight of material being reclaimed will not be able to be determined. In this case after a day of normal production, remove inspection hatch on hopper of collector and see if hopper is empty.









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If not adjustments will need to be reclaim more frequently. Consult factory on recommendations of appropriate changes to timer settings that need to be made.

#### FIELD MAINTENANCE

#### DAILY

- -Observe dust collector operation for leaks and dust escaping from pickup point.
- -Inspect reclaim system for proper operation.
- -Inspect all guards to assure they are in place.
- -Observe and record Magnehelic Gauge reading.

#### WEEKLY

- -Check blower from any vibration.
- -Observe operation of pulse jet valves for proper operation.

#### MONTHLY

- -Inspect interior of collector and bags for any leaks, build up and plugging.
- -Inspect ducting for any leaks, build up and plugging.

#### **FIELD ADJUSTMENT**

Best performance of the dust collector is obtained by observing the magnehelic gauge on a timely basis (frequently at first and, as a steady state condition is established, a daily basis). Adjustment should be made to the timer with the following considerations:

- \* Since the dust collector is more or less continuously cleaned (one row out of 8 at every 30 seconds) there should not be a big change in the magnehelic gauge reading after a pulse.
- \* If blower is turned off for a period of time and restarted, there should be a noticeable drop in gauge reading compared to normal. High drop in gauge reading indicates the bags were too dust covered. Low drop in gauge reading indicates the bags are being over cleaned.
- \* Obtaining the best performance is best done by adjusting OFF TIME. Increase OFF TIME to decrease cleaning cycles and save compressor air.

#### SPARE PARTS

Parts should be ordered from Manufacturer to insure compatibility. If parts are needed, obtain serial number from the name plate and call the factory. A complete detailed record of the vent is on file at CON-E-CO.

#### SAFETY INFORMATION

CON-E-CO dust collectors, like other industrial equipment, must be operated and maintained in accordance with our instructions and sound engineering practices. The user of this equipment must always be aware of the physical and chemical properties of the dust particles being collected. Materials or processes presenting such hazards must be identified by the user.









#### **ELECTRICAL REQUIREMENTS**

It is very important to keep your electric utility company coordinated with your power requirements. The equipment listed below should be combined with other site loads such as area lighting, charging equipment, office HVAC, mixers, etc. If you are using an on site generator, we would be happy to coordinate a more detailed analysis of voltage stabilization and locked rotor amps with the company you select to supply the generator. Transformer sizes listed below assume a 96% eff., an impedence of .035 to calculate voltage drop, the largest motor is Code G, and show standard available size 3 phase transformers.

Setup for 460 Volt operation.

Setup Ioi		V OIL O	P O	,,,,,		Commence of the Commence of th	
CONCRETE BATCH				Wire Size			
	HP	FLA	CB	Str	Heater	Min	Normal
15 KVA Transformer		32.61					
Cement 1 Feed A	40.00	47.60	90	#3	CC74.6	6	6
Cement 1 Feed B	15.00	17.90	45	#2	B32	10	4
Cement Batcher	30.00	34.30	80	#3	CC59.4	8	8
Agg Incline Conv. 1A	25.00	29.60	70	#2	B56	8	8
Agg Incline Conv. 1B	25.00	29.60	70	#2	B56	8	8
Agg Batcher Belt	25.00	*29.60	70	#2	B56	8	8
L. P. Blower	4.50	5.50	15	#0	B8.20	14	10
Airlside Blower	7.00	8.00	20	#1	B12.8	14	8
Air Compressor	25.00	29.60	70	#2	B56	8	8
Water Pump 1	15.00	17.90	45	#2	B32	10	4
Water Pump 2	3.00	4.20	15	#0	B6.25	14	12
PJ 1400 Blower	20.00	24.40	60	#2	B40	8	8
Cement 2 Screw	40.00	*47.60	90	#3	CC74.6	6	6
Chiller	25.00	29.60	70	#2	B56	8	8
Radial Conveyor	40.00	47.60	90	#3	CC74.6	6	6
Transversing Drive	3.00	4.20	15	#0	B6.25	14	12
If not all motors run concurrently, *Amps not included in total.							
Total Connected	342.50	362.61					
+25% of Largest Mot	40.00	11.90				Actual	
Running Design Load		374.51	Runnir	ng Des	sign	298.38	KVA
+5 x Largest Motor		238.00					
Starting Design Load		612.51	Startin	g Des	ign	488.00	KVA
300 KVA Transf. Volt Drop	5.93%	Starting,	and		3.63%	when runn	ing.
500 KVA Transf. Volt Dro		Starting,			2.18%	when runn	ing.

AUX. MIXING EQUIF	MENT					Wire Size	
	HP	FLA	СВ	Str	Heater	Min	Normal
1.5 KVA Transformer		3.3		-951 21 11			
Mixer Drive 1A	75.00	83.4	125	#4	CC132	1	1
Mixer Drive 1B	75.00	83.4	125	#4	CC132	1	1
Hydraulic Pump	50.00	57.7	100	#3	CC94.0	4	4
Total Connected	200.00	227.8					
+25% of Largest Mot	75.00	20.9				Actual	
Running Design Load		248.6	Runn	ing De	sign	198.07	KVA
+5 x Largest Motor		417.0					
Starting Design Load		665.6	Startir	ıg Des	ign	530.31	KVA
225 KVA Transf. Volt Dro		Starting	•		3.21%	when runn	U
300 KVA Transf. Volt Dro	6.45%	Starting	, and		2.41%	when runn	ing.

GRAND TOTAL  HP FLA									
Total Connected	542.50	590.37							
+25% of Largest Mot	75.00	20.85		Actual					
Running Design Load		611.22	Running Design	486.97	KVA				
+5 x Largest Motor		417.00							
Starting Design Load		1028.22	Starting Design	819.20	KVA				
300 KVA Transf. Volt Drop	9.96%	Starting,		2% when runni	ng.				
Note: This will create a	62.32%	continuou	s overload w/listed i	tems.					
500 KVA Transf. Volt Droเ	5.98%	Starting,	and 3.5	55% when runni	ng.				
600 KVA Transf. Volt Drop	4.98%	Starting,	and 2.9	96% when runni	ng.				